

Introduction

- Wax deposition in crude-oil pipelines occurs when temperature drops below WAT, causing buildup that increases pressure drop and reduces flow. Current testing methods are limited or costly. This project develops a lab-scale flow loop to simulate conditions and measure wax behavior in a controlled, repeatable way.

Objectives

- Develop a lab-scale flow loop that simulates pipeline conditions, generates controlled wax deposition, and measures pressure drop and wax thickness.
- Provide a repeatable and reliable testing platform to evaluate wax mitigation methods for research and industry applications.

Constraints

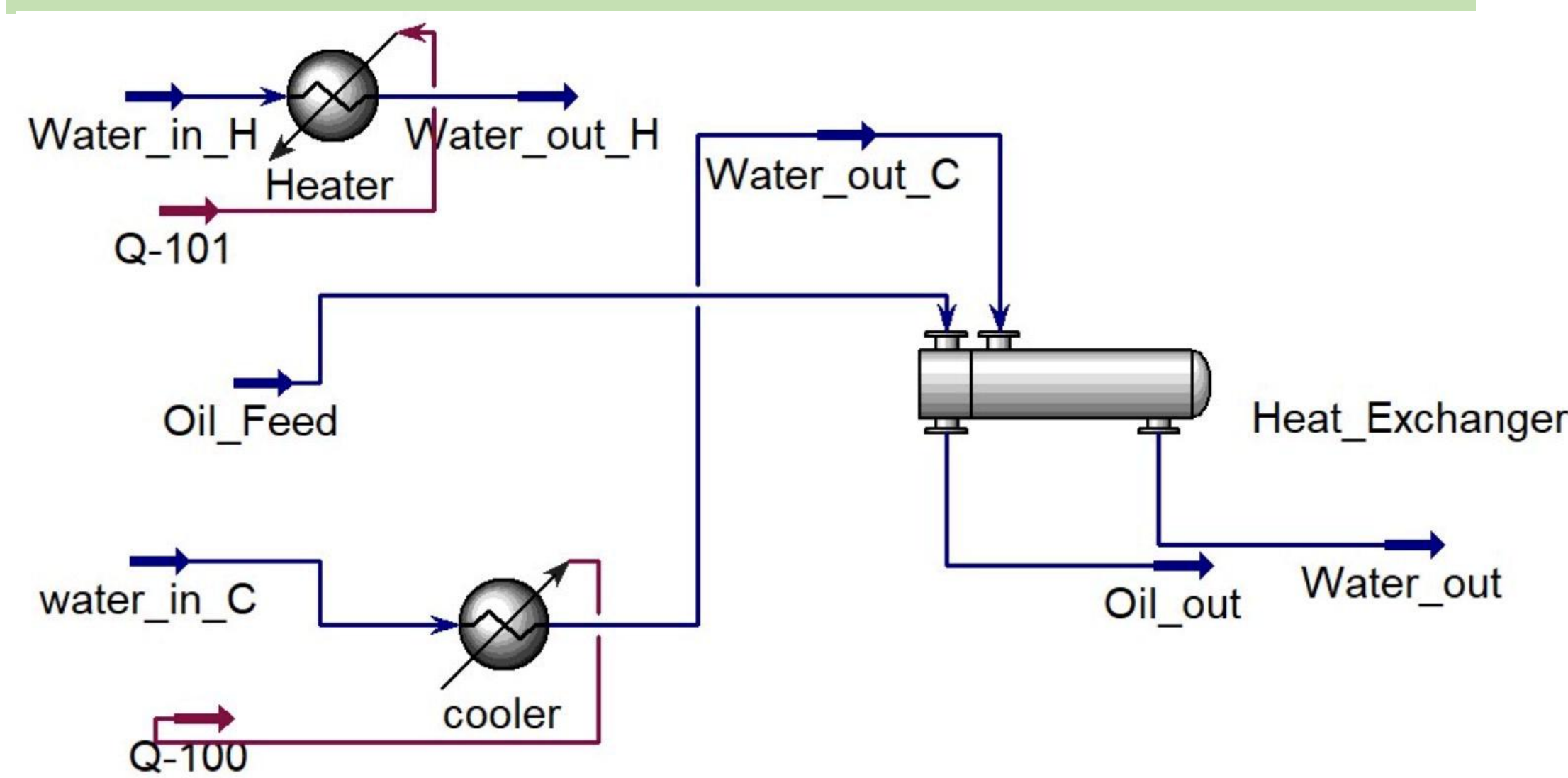
- Must comply with OSHA lab safety standards.
- Use corrosion-resistant materials.
- Must allow complete wax removal.
- Materials must be hydrocarbon compatible.

- Results must be presented in tabulated form.
- Bulk temperature must cross WAT during testing.
- Use only waxy crude or validated model oil.

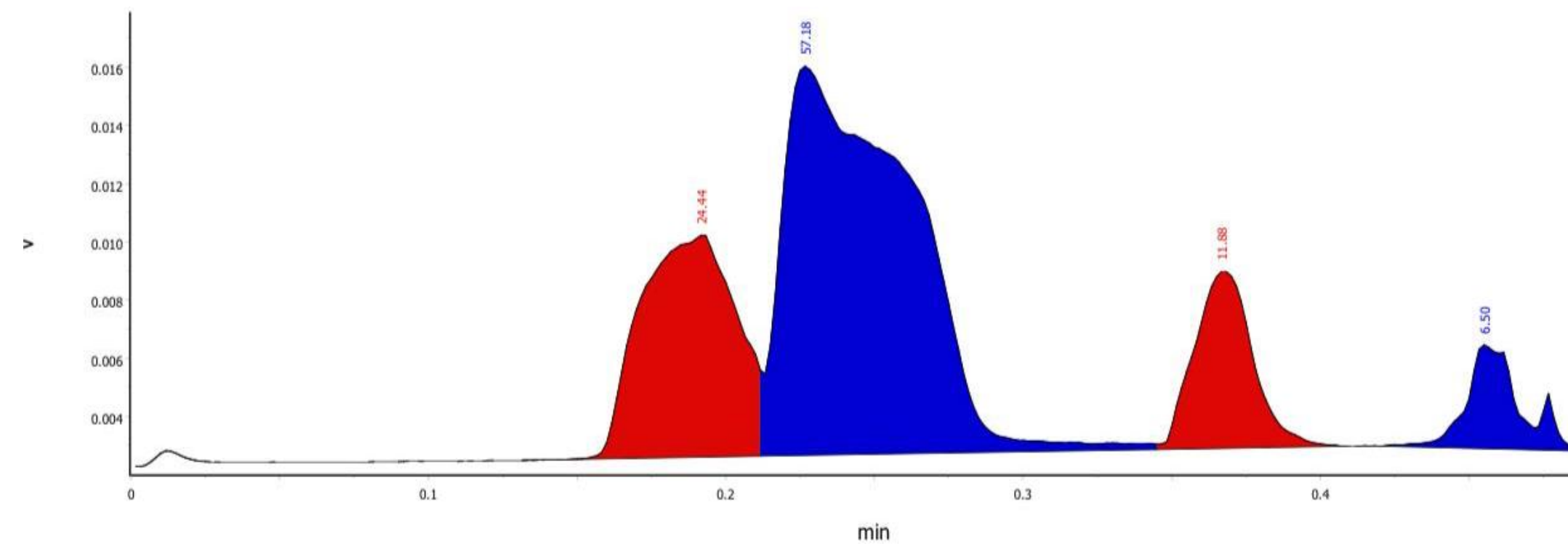
Specifications

- Flow velocity: 0.1 – 7 m/s
- Pressure: 1 – 20 bar
- Represent crude behavior in C20–C44 range
- Footprint: $\leq 4 \text{ m}^2$
- Temperature control: 20–80°C ($\pm 0.5^\circ\text{C}$)
- Cleaning/reset time: $\leq 60 \text{ min}$
- Include over-pressure & over-temperature interlocks

Design Verification

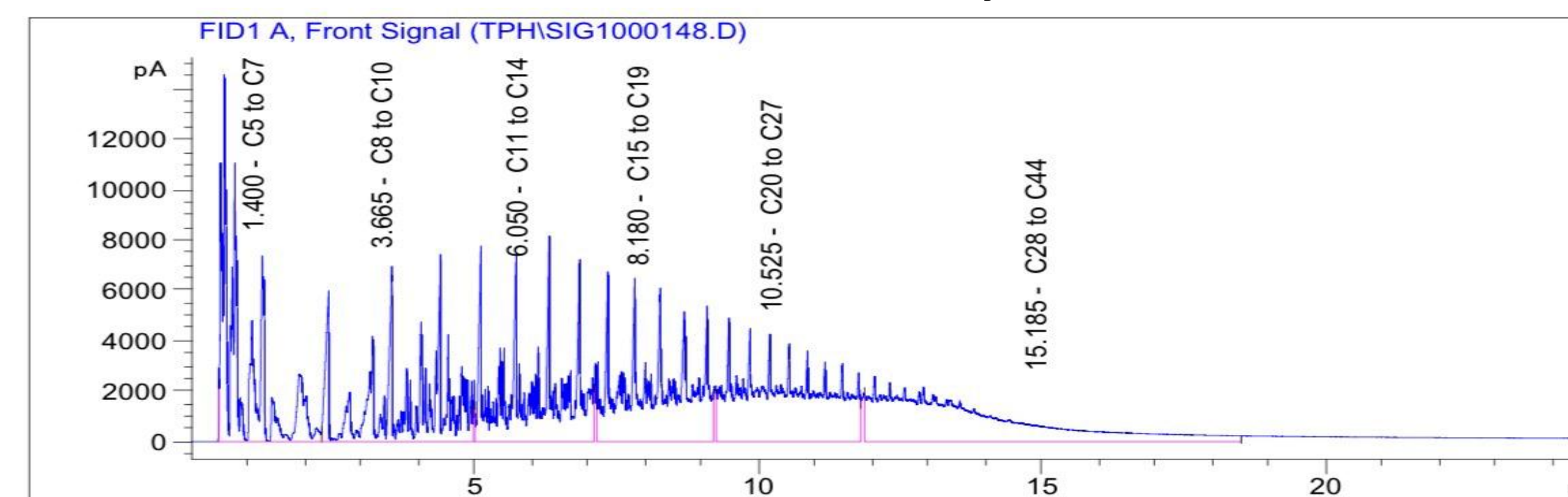


Aspen-hysys Heat Exchanger Simulation



Peak	Fill	Peak Name	ts	ts	ts	H (V)	Hnorm	A (V.S)	Asym	Wo	Asym	Effic	Res	T	Amount
1			0.19	0.13	0.21	0.01	24.90	0.02	24.44						
2			0.23	0.21	0.34	0.01	43.64	0.04	57.18						
3			0.37	0.34	0.41	0.01	19.80	0.01	11.88	0.04	1.24	1659		DB	
4			0.86	0.42	0.69	0.00	11.65	0.00	6.50	0.04	1.84	2220	2.38	RB	

Crude-Oil SARA Analysis



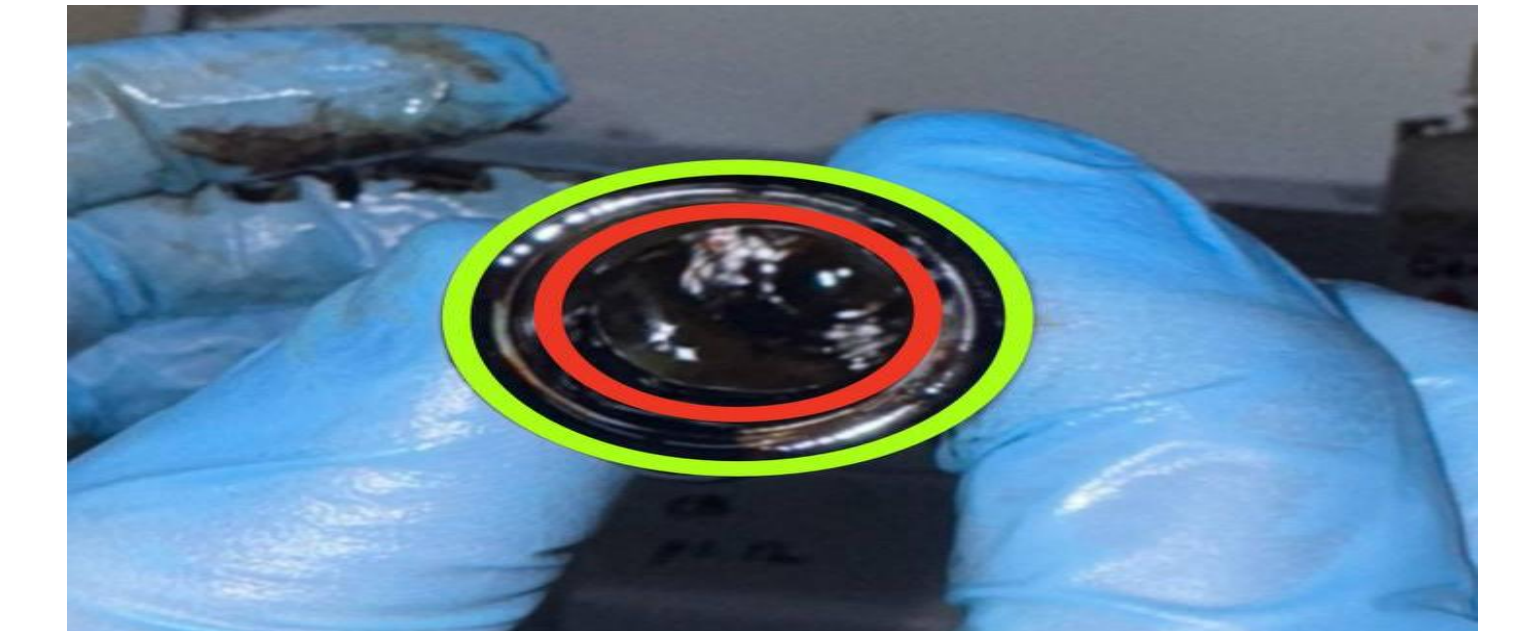
This is a result compounds table. Use the footer button in the table format dialog box to define the summations in the last table line.

#	Exp.RT	Meas.RT	Compound Name	Main Peak Area %
1	1.423	1.400	C5 to C7	14.138
2	3.670	3.665	C8 to C10	13.625
3	6.050	6.050	C11 to C14	15.093
4	8.180	8.180	C15 to C19	16.830
5	10.550	10.525	C20 to C27	20.079
6	15.185	15.185	C28 to C44	20.236

Crude-Oil GC Test

Test Validation

Time min	Temperature	CFlow	L min	Flow m3 s	drailic	Effective Diameter	velocity m	Pressure Drop	ps	Pressure Drop	balpstream	Pressure	pspstream	Pressure	balax	Thickness mm
49	26.1	4.09	0.000068		10.000	0.868	1.644	0.113	19.644	1.354	0.000					
50	26.1	4.09	0.000068		10.000	0.868	1.644	0.113	19.644	1.354	0.000					
51	26.0	4.09	0.000068		10.000	0.868	1.644	0.113	19.644	1.354	0.000					
52	26.0	4.09	0.000068		10.000	0.868	1.644	0.113	19.644	1.354	0.000					
53	25.9	4.11	0.000069		9.894	0.892	1.726	0.119	19.726	1.360	0.151					
54	25.9	4.14	0.000069		9.793	0.915	1.808	0.125	19.808	1.366	0.295					
55	25.8	4.16	0.000069		9.697	0.938	1.890	0.130	19.890	1.371	0.452					
56	25.7	4.18	0.000070		9.606	0.961	1.973	0.136	19.973	1.377	0.563					
57	25.7	4.20	0.000070		9.519	0.983	2.055	0.142	20.055	1.383	0.687					
58	25.6	4.22	0.000070		9.437	1.005	2.137	0.147	20.137	1.388	0.804					
59	25.6	4.23	0.000071		9.358	1.026	2.220	0.153	20.220	1.394	0.917					



Physical Prototype



Conclusion

- The system demonstrated stable and repeatable operation.
- Clear pressure-drop increases were observed during wax deposition.
- The flow loop effectively replicates real pipeline conditions.
- The system provides consistent data for analyzing wax deposition behavior.